

C1  
portion having a Melt Flow Rate ( $MFR_2$ ) of more than 0.5/10 min.  
The polymer has a Melt Flow Rate ( $MFR_2$ ) of 0.1 to 20g/10 min.

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The paragraph beginning on page 8, line 34, has been amended as follows:

C2 Examples of suitable catalyst systems are described in, for example, Finnish Patent Nos. 86866, 96615 and 88047 and 88048.

The paragraph beginning on page 8, line 36, has been amended as follows:

C3 One particularly preferable catalyst, which can be used in the present invention, is disclosed in FI Patent No. 88047. Another preferred catalyst is disclosed in Finnish Patent Application No. 963707.

The paragraph beginning on page 11, line 32, has been amended as follows:

C4 The catalyst can be prepolymerized prior to feeding into the polymerization reactor. During prepolymerization the catalyst components are contacted for a short period with a monomer, such as an olefin monomer, before feeding into the reactor. Examples of suitable systems are described in, e.g., Finnish Patent Application No. 961152. It is also possible, as described in Finnish Patent No. 95387, to carry out the prepolymerization in the presence of a viscous substance, such as an olefinic wax or an oil/wax mixture, to provide a prepolymerized catalyst which is stable during storage and handling. The catalysts prepolymerized in wax will also allow for easy dosing of the catalyst into the

*Cm C*  
polymerization reactors.

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The paragraph beginning on page 21, line 24, has been amended as follows:

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*C 5*  
The polymerizations were carried out in the presence of a Ziegler-Natta catalyst with an external electron donor corresponding to the general formula I and V above (dicyclopentyl dimethoxy silane, in the following abbreviated "D"). The catalyst was prepared according to the method described in FI Patent No. 88047. A polymer prepared in the presence of a corresponding catalyst system containing a conventional donor corresponding to the general formula IV (cyclohexyl methyl dimethoxy silane or abbreviated "C") was tested. As a reference, a commercial polypropylene was used. Polymerizations were made in liquid propylene where the first polymerization step was made without any hydrogen in the feed and the second step in the presence of hydrogen.

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The paragraph beginning on page 23, line 16, has been amended as follows:

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*C 6*  
A prepolymerized  $MgCl_2$  supported Ti-catalyst (prepared according to FI Patent No. 88047 was used in the polymerization. The cocatalyst was triethyl aluminium (TEA) and dicyclopentyl dimethoxy silane (DCPDMS) was used as an external donor. The Al/Ti mole ratio was 150 and Al/donor mole ratio 5.

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Please add the following paragraph on page 5, line 7 of the Specification: